

# Application of a Heat Integrated Post-combustion CO<sub>2</sub> Capture System with Hitachi Advanced Solvent into Existing Coal-Fired Power Plant

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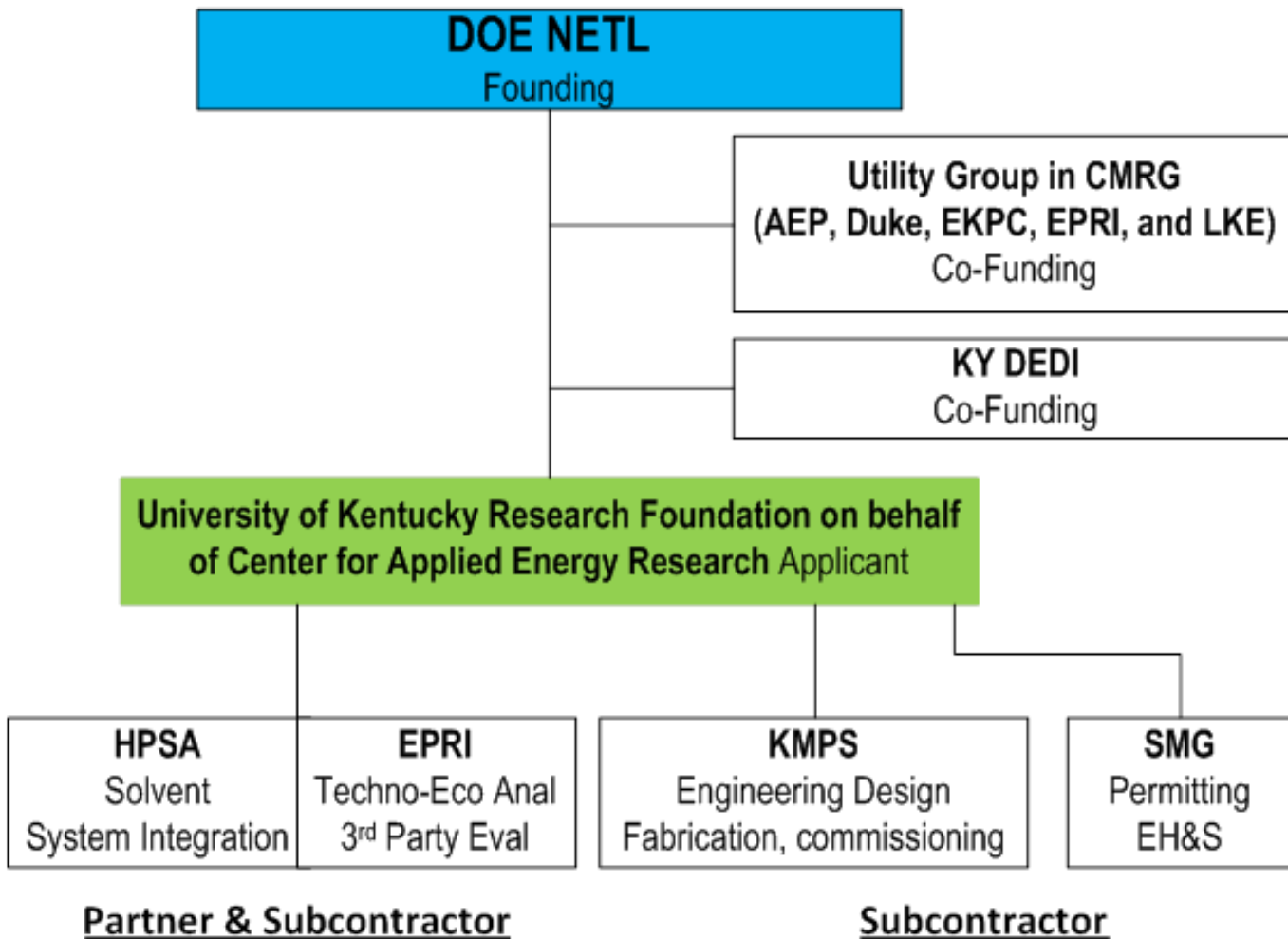
Main CAER Facility Located Off-campus in Lexington, KY  
(est. 1977)  
162 employees, \$12M Budget



UK's first LEED Research Laboratory  
\$19.8 M Renewable Energy Lab  
(finished in June)

- Project Funding:
  - \$14.55M from DOE NETL
  - \$ 4.73M cost share from team, KY DEDI and CMRG
    - \$0.78M from team
    - \$3.65M from KY DEDI
    - \$0.3M from Carbon Management Research Group (CMRG)
- 4-year project consisting of 4 budget periods

- Overall Performance Dates (no-cost extension is in progress):
  - BP-1 October 1, 2011 to August 31, 2012
  - BP-2 September 1, 2012 to January 31, 2013
  - BP-3 February 1, 2013 to January 31, 2014
  - BP-4 February 1, 2014 to January 31, 2016



- EPRI

- Abhoyjit Bhowan
- Dick Rhudy
- George Booras
- Andrew Maxson
- David Thimsen
- Ron Schoff

- HPSA

- Song Wu
- Sandhya Eswaran

- KMPS

- Tom Schafer
- Stan Lam
- Allyson Chazen

## LKE

- John Moffett
- David Link
- Jeff Fraley
- Donald Duncan

## SMG

- Sara Smith
- Clay Whitney

## UKRF

- Kunlei Liu
- Jim Neathery
- Joe Remias
- Lisa Richburg
- Heather Nikolic
- Jesse Thompson
- Others

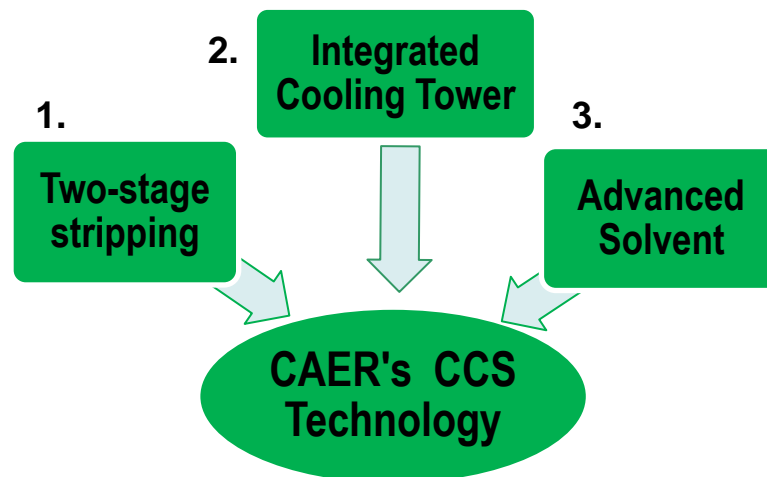
## Worley-Parsons

- Jacqueline Bird
- Mike Bartone

- 1) To gather data on solvent degradation kinetics, water management as well as other information during the long-term verification runs;
- 2) To provide scale-up data and design information for commercial-scale projects;
- 3) To demonstrate a heat-integrated post-combustion CO<sub>2</sub> capture system with advanced solvent; and
- 4) To collect information/data on material corrosion and identify appropriate materials for a 550 MWe commercial-scale carbon capture plant.

Engineering design, build and install an advanced CO<sub>2</sub> capture system into an existing PC power plant at a 0.7 MWe slipstream scale (~15 TPD CO<sub>2</sub>)

Three novel processes will be designed and integrated: 2-stage solvent stripping, cooling tower desiccant, and Hitachi solvent



## 1. Two-stage Stripping:

- Increase solvent working capacity by providing a secondary air-stripping column following the conventional steam stripping column.
- Air stripping stream sent to boiler as combustion air to increase flue gas P<sub>CO<sub>2</sub></sub> exiting boiler

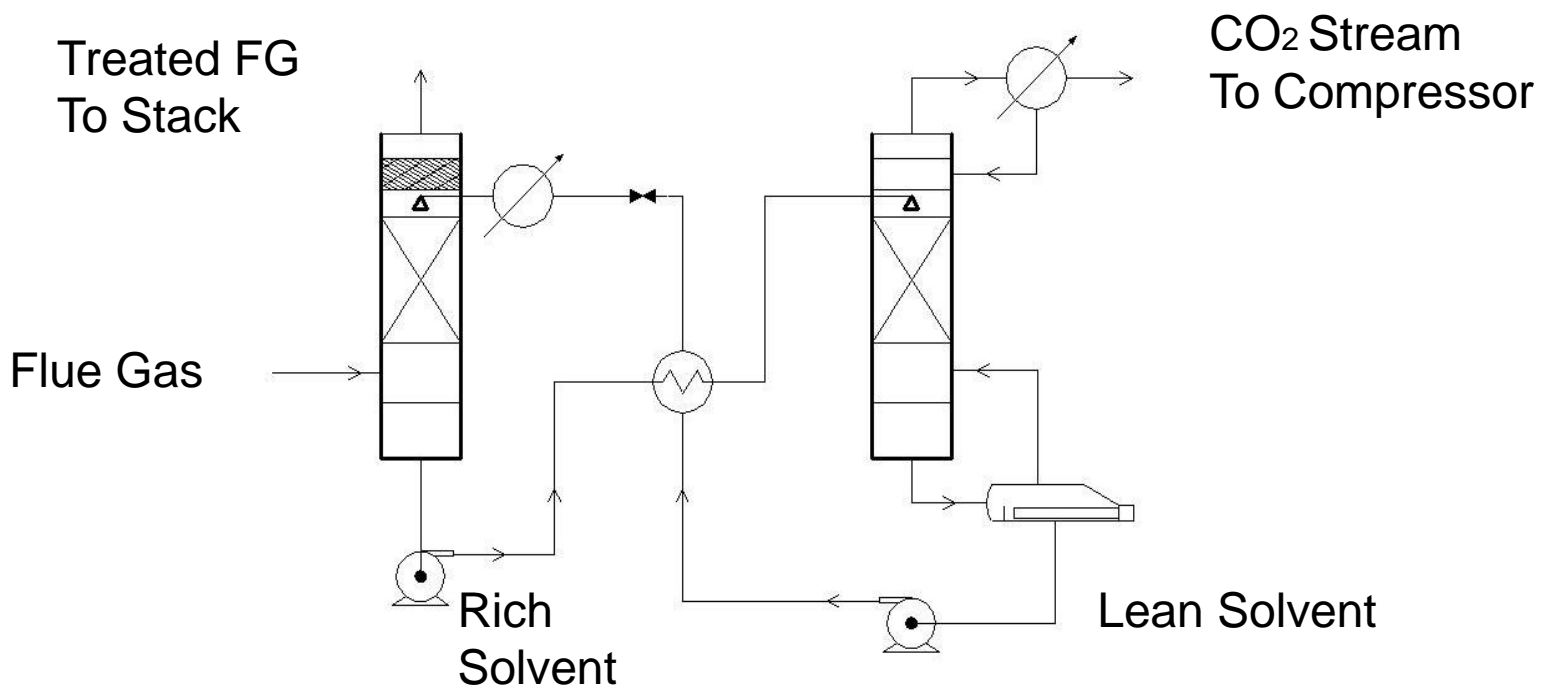
## 2. Integrated Cooling Tower:

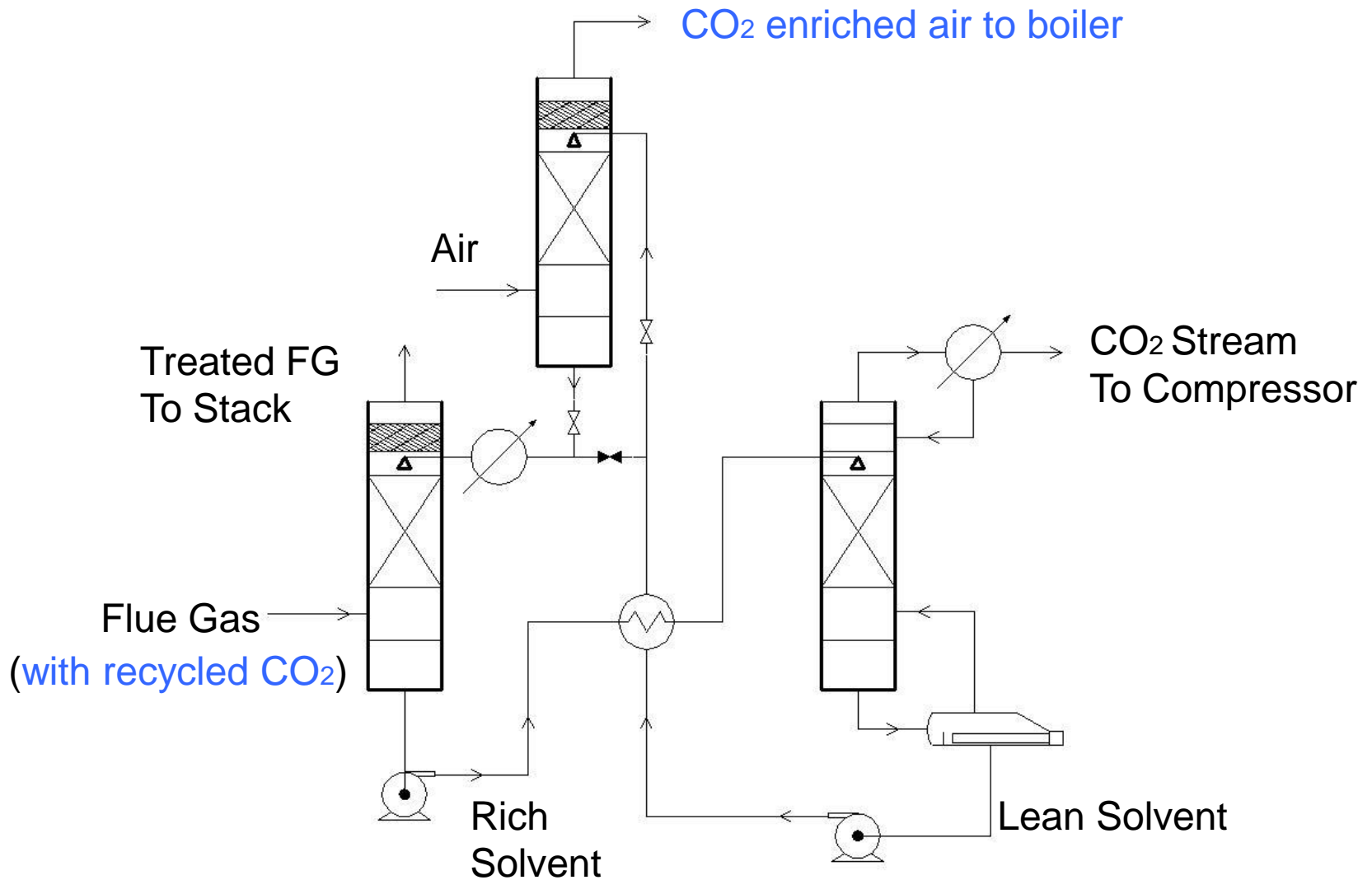
- Use regenerated CO<sub>2</sub> stream waste heat to dry liquid desiccant
- Liquid desiccant is used to dry cooling tower air → Improved power plant cooling tower and steam turbine efficiency

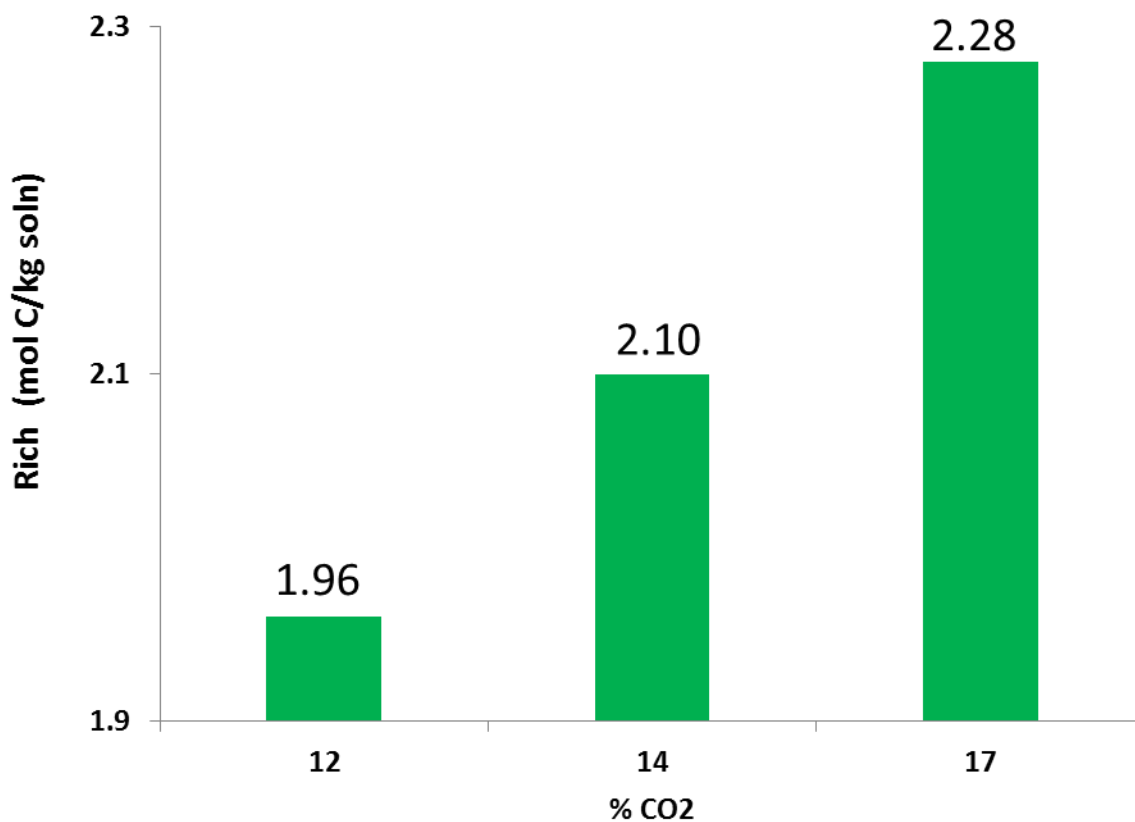
## 3. Advanced Hitachi Solvent:

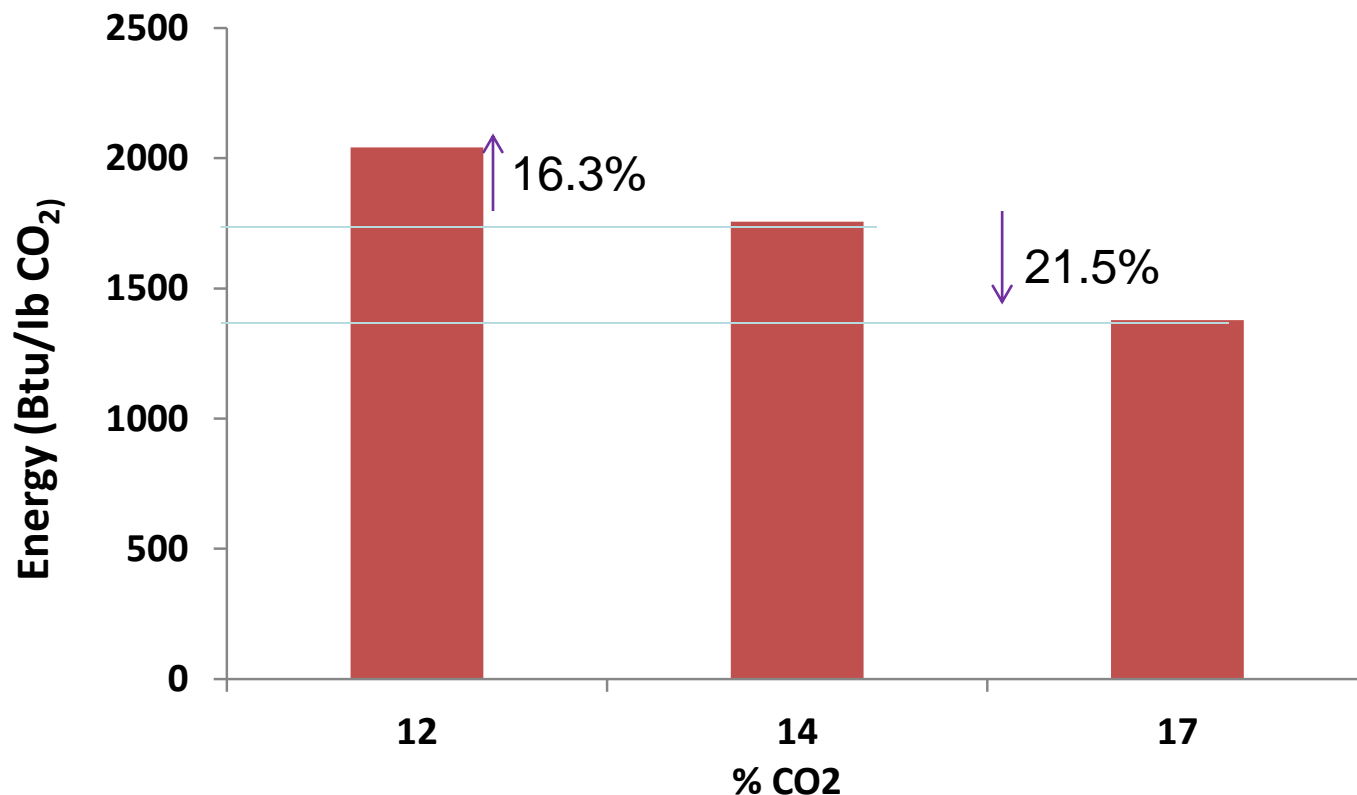
- Primary amine analogous to MEA

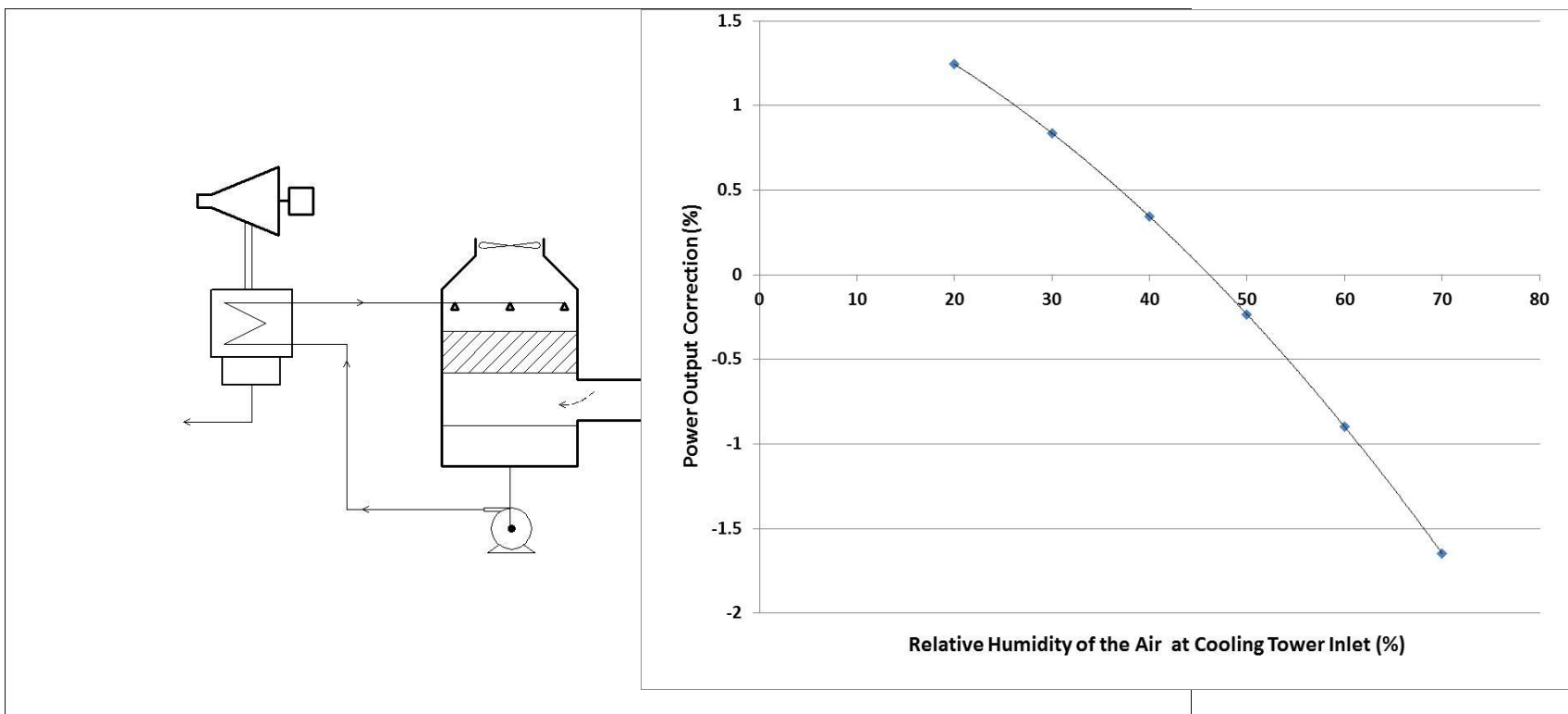


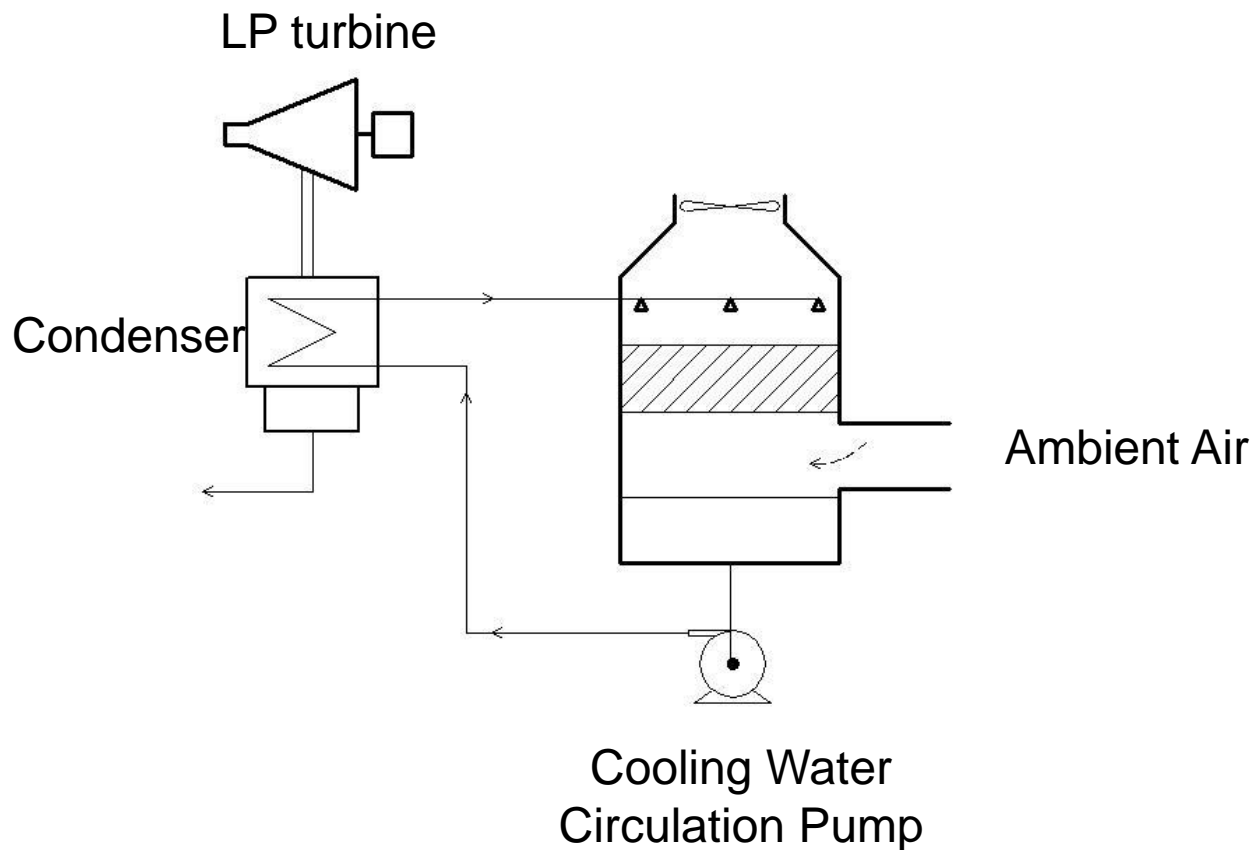


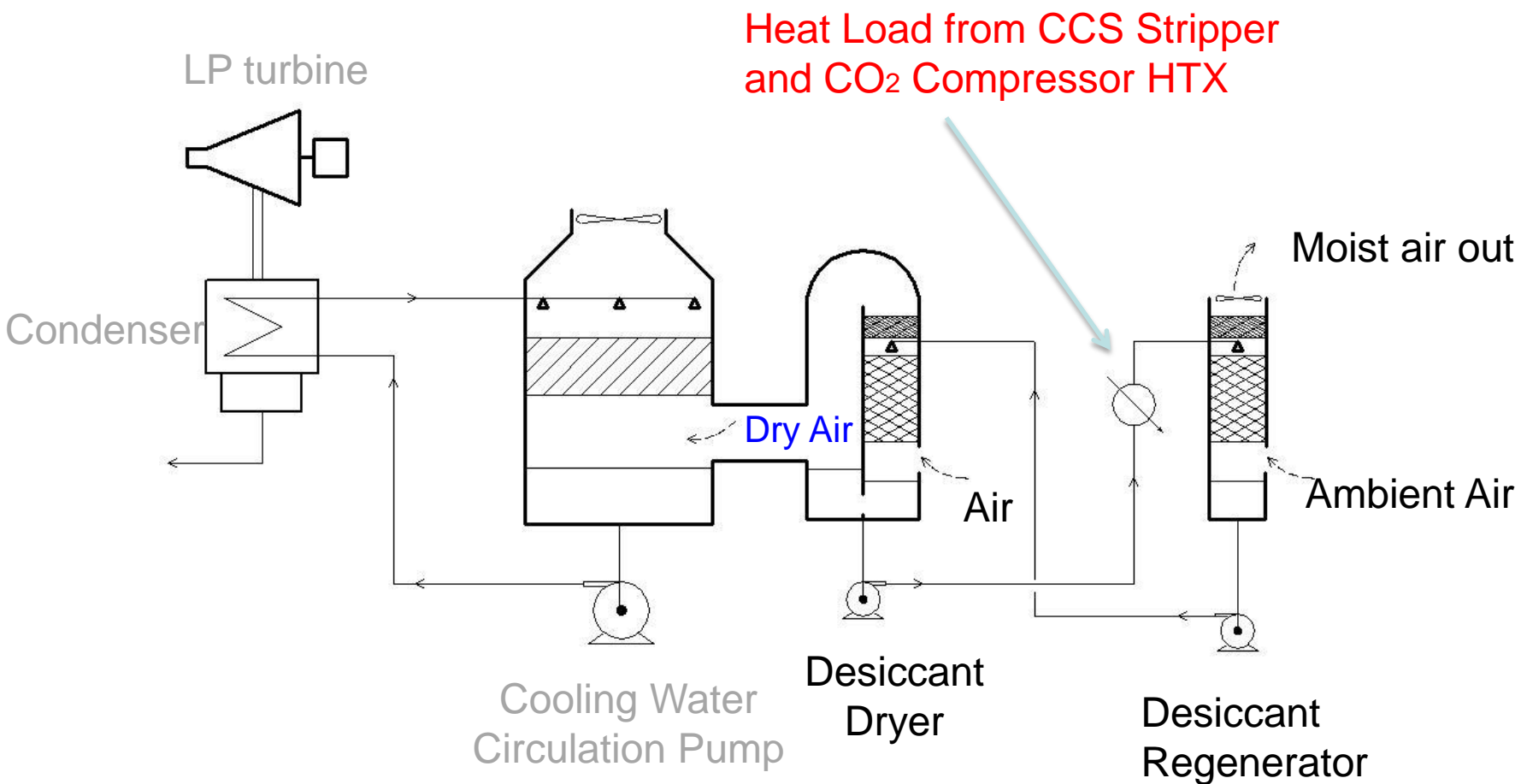


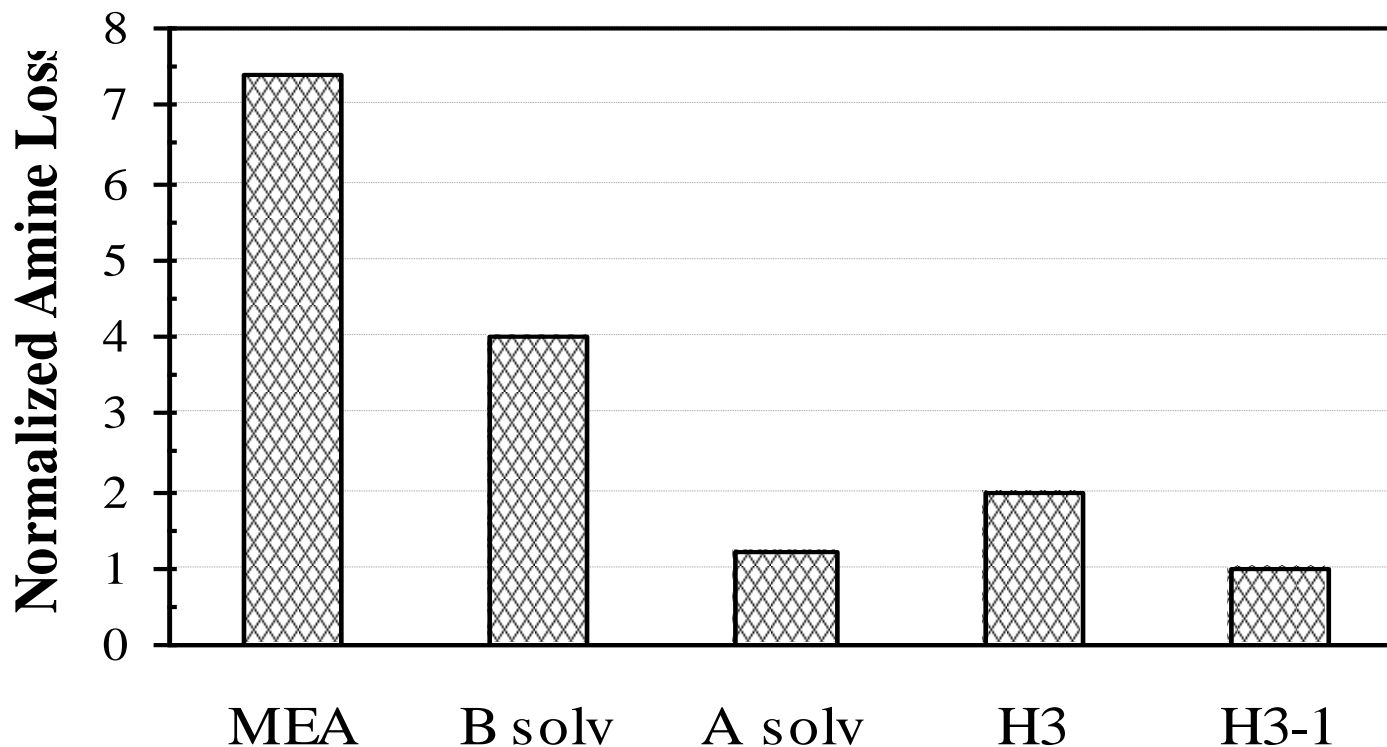














- The design, start-up/commissioning of a 2MWth test facility (1400cfm);
- Parametric investigation and long-term verification;
- New corrosion resistance coatings for material used in CCS system (access ports needed in scrubber and stripper areas);
- Solvent degradation (liquid product and gaseous emissions from CCS);
- A series of transient tests to quantify the ability of the carbon capture system to follow load demand.

- Located at 815 Dix Dam Rd, Harrodsburg, KY 40330
- 40 miles from UKy-CAER



- Unit 1: B&W wall fired sub-critical boiler with Westinghouse 110 (gross) MW reheat turbine (1450 psig/1000°F/1000°F), ESP, and Low NOx burners;
- Unit 2: CE t-fired sub-critical boiler with Westinghouse 180 MW (gross) reheat turbine (1800 psig /1000°F /1000°F), ESP, Low NOx burners, and OFA;
- Unit 3: CE t-fired sub-critical boiler with Westinghouse 457 MW (gross) reheat turbine (2400 psig/1000°F /1000°F), ESP, Low NOx burners, and OFA.
- FGD common to all 3 units, in near future, SCR and SAM Mitigation Equipment.

# Possible Test Coals During the Investigation

- Illinois/Western Ky bituminous (high sulfur)

Proximate Analysis	As-Received
% Moisture	14.3-16.3
% Ash	8.5-9.8
% Volatile	34.2-36.4
% Fixed Carbon	39.7-40.9
BTU	10580-11111
MAF BTU	14320-14431
% Total Sulfur	2.77-3.52
<b>Sulfur Forms</b>	
% Pyritic	1.4-1.9
% Sulfate	0.03-0.04
% Organic	1.4-1.6

Ultimate Analysis	As-Received
% Moisture	14.51
% Carbon	60.79
% Hydrogen	4.29
% Nitrogen	1.31
% Chlorine	*****
% Sulfur	3.28
% Ash	8.5
% Oxygen (Diff.)	7.32
Chlorine D6721 Dry Basis $\mu\text{g/g}$ 117	

Mineral Analysis	% Ignited Basis
Phos. Pentoxide, $\text{P}_2\text{O}_5$	0.17
Silica, $\text{SiO}_2$	41.4
Ferric Oxide, $\text{Fe}_2\text{O}_3$	29.79
Alumina, $\text{Al}_2\text{O}_3$	20.16
Titania, $\text{TiO}_2$	0.93
Lime, CaO	1.31
Magnesia, MgO	0.79
Sulfur Trioxide, $\text{SO}_3$	1.05
Potassium Oxide, $\text{K}_2\text{O}$	1.89
Sodium Oxide, $\text{Na}_2\text{O}$	0.43
Barium Oxide, BaO	0.05
Strontium Oxide, SrO	0.03
Manganese Dioxide, $\text{Mn}_3\text{O}_4$	0.04
Undetermined	1.96

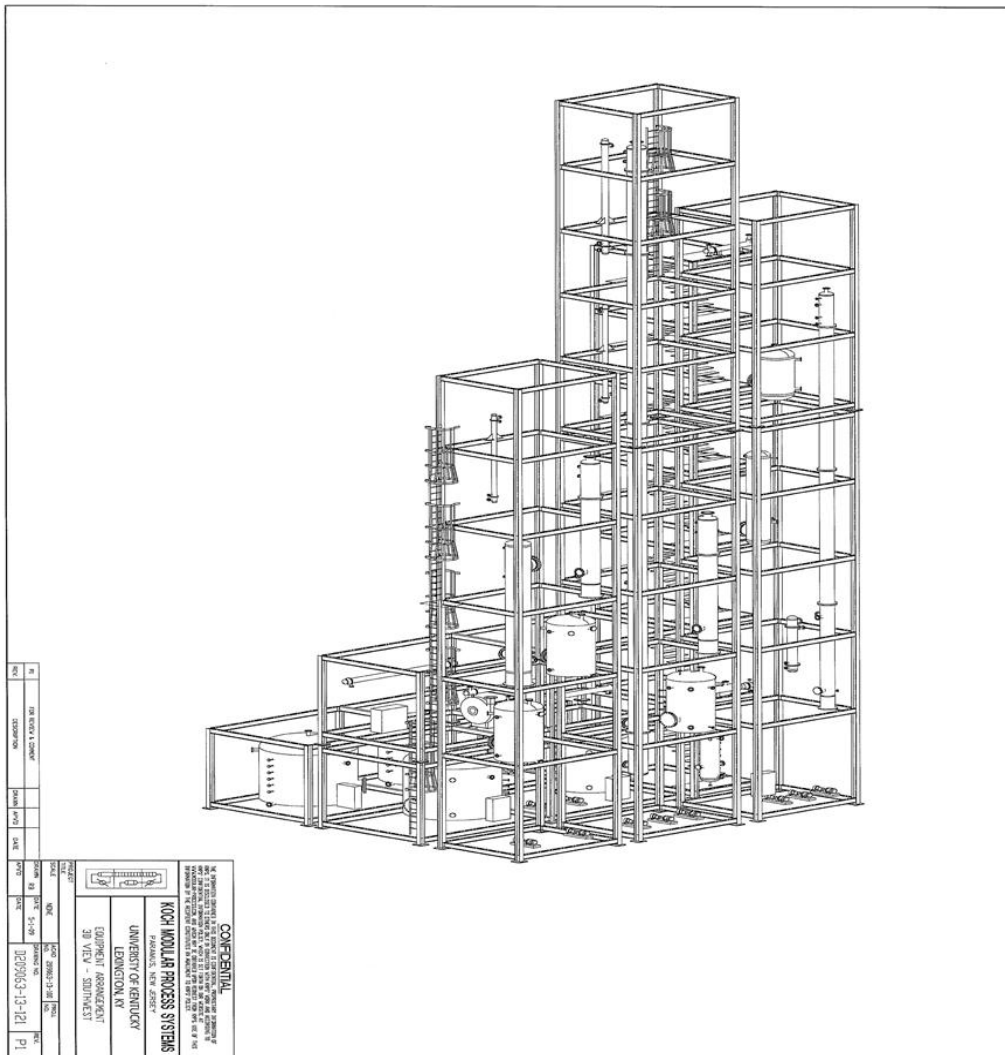
BP	Task	Name
	1.0, 5.0, 9.0, 17.0	<b>Project Management &amp; Planning</b>
1	2.0	<b>System and Economic Analysis.</b>
	3.0	<b>Initial EH&amp;S Assessment</b>
	4.0	<b>Basic Process Specification and Design</b>
2	6.0	<b>Slipstream Site Suvery</b>
	7.0	<b>Finalized Engineering Specification and Design</b>
	8.0	<b>Test Condition Selection and Test Plan</b>
3	10.0	<b>System Engineering Update and Model Refinements</b>
	11.0	<b>Update of EH&amp;S Assessment</b>
	12.0	<b>Site Preparation</b>
	13.0	<b>Fabrication of Slip-stream Modules</b>
	14.0	<b>Procurement and Installation of Control Room/Field</b>
	15.0	<b>Fabrication of Corrosion Coupons</b>
	16.0	<b>Slipstream Facility Erection, Start-up, Commissioning</b>
4	18.0	<b>Slip-stream Test Campaign</b>
	19.0	<b>Final Updater of Techno-Economic Analysis</b>
	20.0	<b>Final EH&amp;S Assessment</b>





Raw Flue Gas Data at MCR-GR Unit 3		
CO <sub>2</sub>	% vol.	12.2
H <sub>2</sub> O	% vol.	8.9
N <sub>2</sub>	% vol.	
O <sub>2</sub>	% vol.	5.1
NO <sub>x</sub> @ 6% O <sub>2</sub> dry	Lb/mmBtu	0.452
CO @ 6% O <sub>2</sub> dry	ppmv	
SO <sub>2</sub> @ 6% O <sub>2</sub> dry	ppmv	1,110.00
NH <sub>3</sub> @ 6% O <sub>2</sub> dry	ppmv	
PM @ 6% O <sub>2</sub> dry	mg/Nm <sup>3</sup>	
Flue Gas Temperature	°F	300
Flue Gas Pressure	psia	
Flue Gas Flow to CCU	WSCFH	23,180,667

Note: Slip-stream extraction will be at the combined scrubber exit.



- 80 ft tall
- 1000 ft<sup>2</sup> footprint  
(15'x65', but could be rearranged)
- 5 to 6 modules with 100,000lbs/module
- Plus control/lab trailer and others

- Finalized budget for duration of project
- Finalized contract with UKy and DOE
- PSC with Smith Management Group (SMG)
- Several visits to Brown Station
- Finalized host site agreement with LKE
- Preliminary design with Aspen Plus complete and sent to Hitachi, EPRI, and KMPS for review
- RFP sent to KMPS for review
- Q4 2011 & Q1 2012 reports submitted to DOE
- BP1 continuation submitted to DOE
- Introduced multi-party NDA between all contributing parties
- Last stage of finalizing contracts with subs





- Finish the techno-economic analysis and submit report to DOE
- Finish the EH&S assessment and report
- Work with KMPS to obtain finalized design
- Prepare BP1 end report for DOE

